

AMENDMENTS TO THE CLAIMS:

This listing of claims will replace all prior versions and listings of claims in the application:

Listing of Claims:

1. (Currently Amended) A process for preparing polymer [[/]] or food grade hydrocarbon solvents of naphtha range containing very low aromatics, especially ~~benzene less than 20ppm~~ from naphtha range petroleum stock, said process comprising the steps of:
 - a. heating the naphtha range petroleum feed stock to a temperature in the range of 70° - 180°C;
 - b. adding stoichiometric amount of hydrogen to the naphtha range petroleum feed stock at a pressure between about 5 to 30 bar;
 - c. passing the mixture of step (b) feed and hydrogen through a reactor having a nickel based catalyst;
 - d. removing any excess hydrogen to obtain the polymer [[/]] or food grade hydrocarbon solvents of naphtha range containing very low aromatics.
2. (Currently Amended) [[A]] The process as claimed in claim 1, wherein the naphtha range petroleum feed stock is a preferably raffinate stream obtained from the solvent extraction units employed for recovery of aromatics from reformate.
3. (Currently Amended) [[A]] The process as claimed in claim [[1]] 2, wherein the raffinate [[feed]] stream has sulfur content less than [[<]] 50ppm, ~~preferably < 5 ppm and most preferably < 1 ppm.~~
4. (Currently Amended) [[A]] The process as claimed in claim [[1]] 2, wherein

the raffinate [[feed]] stream has aromatics content less than [[<]] 20% by wt and preferably < 10% by wt.

5. (Currently Amended) [[A]] The process as claimed in claim [[1]] 8, wherein the raffinate [[feed]] stock has benzene content less than < 20% by wt and preferably < 10% by wt.
6. (Currently Amended) [[A]] The process as claimed in claim [[1]] 2, wherein the raffinate [[feed]] stream has boiling point in the range of C₅ to 110°C.
7. (Currently Amended) [[A]] The process as claimed in claim 1, wherein the raffinate [[feed]] stock has boiling point in the range of 63° - 70°C.
8. (Currently Amended) [[A]] The process as claimed in claim [[1]] 2, wherein the raffinate stream has about 4 – 7% by wt benzene.
9. (Currently Amended) [[A]] The process as claimed in claim 1, wherein the nickel based catalyst is nickel-alumina catalyst having nickel supported on alumina catalyst.
10. (Currently Amended) [[A]] The process as claimed in claim 1, wherein the nickel loading on alumina is about 10 to 70% by wt, and preferably is about 30 to 60% by wt.
11. (Currently Amended) [[A]] The process as claimed in claim [[1]] 9, wherein the metal surface area of the nickel-alumina catalyst is about 10 – 20 m²/g.
12. (Currently Amended) [[A]] The process as claimed in claim [[1]] 9, wherein the physical surface area of the nickel-alumina catalyst is about 120 – 200 m²/g and the pore volume of the catalyst is about 0.2 – 0.3 cc/gm.

13. (Canceled).
14. (Currently Amended) ~~[[A]]~~ The process according to claim 1 ~~where-in~~
wherein the polymer or food grade hydrocarbon the product-solvent solvents
thus obtained contains nil olefins, Sulfur less than 1 ppm and ~~aromatics,~~
~~especially, Benzene~~ benzene less than 20 ppm.
15. (Currently Amended) ~~[[A]]~~ The process according to claim 1, ~~where-in~~
wherein the naphtha range petroleum feed stock Feed is a low value raffinate
stream obtained from BTX extraction column e.g.-Udex-unit.
16. (Currently Amended) ~~[[A]]~~ The process according to claim 1, ~~where-in~~
wherein the naphtha range petroleum feed stock has maximum 20 wt%
aromatics and 10 wt% ~~Benzene~~ benzene.
17. (Currently Amended) ~~[[A]]~~ The process according to claim 1, ~~where-in~~
wherein process step (c) is carried out under hydrogen environment at
temperature in the range of preferably at 80 - 150°C, and pressure in the
range of 10 to 20 bar.
18. (Canceled).
19. (Currently Amended) ~~[[A]]~~ The process according to claim ~~[[9]]~~ 1, ~~where-in~~
wherein the nickel based Oxided-Ni catalyst is oxidized and pre-reduced
before loading into the reactor.
20. (Canceled).
21. (New) The process as claimed in claim 3, wherein the raffinate stream has

sulfur content less than 5 ppm.

22. (New) The process as claimed in claim 3, wherein the raffinate stream has sulfur content less than 1 ppm.
23. (New) The process as claimed in claim 4, wherein the raffinate stream has aromatics content less than 10% by wt.
24. (New) The process as claimed in claim 10, wherein nickel loading on alumina is about 30 to 60% by wt.
25. (New) The process as claimed in claim 15, wherein the BTX extraction column is an Udex unit.